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PATENT

IN THE UNITED STATES DESIGNATED OFFICE (DO/US)

In re: David Miles  
Serial No.: 10/624,441  
Filing Date: July 22, 2003  
For: **RENDERING SCREW PRESSES AND METHODS OF OPERATING THE SAME**

Confirmation No.: 6411  
Group Art Unit: 3725  
Examiner: Jimmy T. Nguyen

Date: July 7, 2005

MAIL AMENDMENT  
Commissioner for Patents  
Post Office Box 1450  
Alexandria, Virginia 22313-1450

**SUBMITTAL OF PRIORITY DOCUMENT**

Sir:

To complete the requirements of 35 USC 119, enclosed is a certified copy of the following UK priority application:

GB0306283.3, filed March 19, 2003.

Respectfully submitted,

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1. Your reference

SPG/P101880GB

2. Patent application number

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0306283.3

3. Full name, address and postcode of the or of each applicant (*underline all surnames*)De Smet Rosedowns Limited  
Cannon Street  
HULL  
HU2 0AD  
East YorkshirePatents ADP number (*if you know it*)

If the applicant is a corporate body, give the country/state of its incorporation

6611461001

4. Title of the invention

Improvements to Rendering Presses

5. Name of your agent (*if you have one*)

Harrison Goddard Foote

"Address for service" in the United Kingdom to which all correspondence should be sent (*including the postcode*)31 St Saviourgate  
YORK  
YO1 8NQPatents ADP number (*if you know it*)

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7. If this application is divided or otherwise derived from an earlier UK application, give the number and the filing date of the earlier application

Number of earlier application

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Description 7

Claim(s) 7

Abstract 1

Drawing(s) 2 *only*

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I/We request the grant of a patent on the basis of this application.

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Date

19 March 2003

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S P Gilholm

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### Improvements to Rendering Presses

This invention relates to a novel method of extracting fluids from oil or fat bearing materials, such as rendered bone material and to novel apparatus related thereto, e.g. a mechanical screw press incorporating a worm assembly.

A number of screw press manufacturers design continuous mechanical screw presses for use in the rendering industry which incorporate a worm assembly rotatably driven by a drive shaft. Conventionally, presses comprise a known worm assembly rotating within a drained "Cage" or tunnel from which oils and/or fats are expelled, e.g. radially.

In use, pre-cooked process material enters the press at a feed end of the press and is subjected to continuously increasing pressure until it is discharged as 'cake' at a discharge end of the press, for example, via an hydraulically-adjustable annular choke assembly. Derivatives of the basic design, incorporating similar worm assemblies and/or similar choke assemblies, are also known.

De Smet Rosedowns (DSR) are UK-based manufacturers of screw presses and spare parts for both the vegetable oil extraction industry and for the rendering industry. Over the years, DSR has been at the forefront of design innovation for improving the performance of screw presses in terms of increased throughput, lower residuals and reduced power consumption. Such improvements rely on an intimate knowledge of press operation and on the ability to predict changing pressure and flow conditions within a press. An important aspect of DSR business is the design and manufacture of performance enhancing worm assemblies for fitting to presses originally manufactured by competitors.

Recent developments in screw presses have tended towards addressing the wear that occurs on the flights of worm assemblies. Thus, for example, European Patent application No. 0 540 222 describes the use of a bi-metallic worm assembly.

However, it should be noted that the design of the worm assembly itself is conventional.

5 Mechanical screw presses find utility in a number of areas, including extraction of oils from seeds and/or nuts and extraction of fats from animal by-products. It will be understood that reference hereinafter to 'process material' should be construed generally as meaning products used in the Rendering Industry, such as animal carcasses.

10 Recent developments in the extraction of oil from seeds, using mechanical screw presses, have utilised a novel multi-stage approach of sequentially pressing, mixing and pressing the seeds. Whilst this method has been found to be advantageous in seed presses, it has hitherto been considered unsuitable for use in rendering screw presses, due, *inter alia*, to the risk of clogging of the mixing portion of the worm  
15 assembly in the screw press.

Nevertheless, we have now surprisingly found that, not only can conventional screw presses be adapted to include a mixing region in the worm assembly, but, in use, this results in a significantly improved yield of oil/fat from the mechanical press.  
20 Recently, a DSR conversion of a Dupps press has yielded dramatic improvements in throughput (around 50%) with no significant deterioration in residual fat levels. Furthermore, no increase in power consumption or wear of critical parts was observed. (measured per ton of material processed) Indeed, in some instances power consumption was reduced.

25 Thus, according to the invention we provide a method of extracting liquids from process material which comprises the sequential steps of compressing the process material; decompressing and mixing the process material; and further re-compressing the process material in a mechanical screw press.

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The step of decompressing and mixing may occur separately, simultaneously or sequentially. In one embodiment described herein decompression and mixing steps may occur separately. In such a case it is preferred that the decompression substantially precedes the mixing. However, in the most preferred embodiment and  
5 the embodiment hereinafter described in the examples, the decompression and mixing occur simultaneously.

The decompression/mixing process can be carried out using a mixer assembly as hereinafter described. However, preferably the decompression/mixing process can be  
10 carried out using a compression mixer. A compression mixer, which may also be referred to as a Hump mixer, is especially advantageous in that, *inter alia*, it will produce an extra compression just prior to the decompression and mixing zone. Thus, it will be understood that a compressor mixer may comprise a frusto conical (compressor) member and an optionally integral mixing member.

15 Extraction of fat in, for example, a Dupps press using the original assembly (Fig 1) is by a process of continuously increasing the pressure applied to the process material as it moves from the intake to the discharge end of the press. However, there comes a point at which the pressure required to expel further fat is disproportionately high.  
20 The DSR worm assembly (Fig 2) relies on the principle analogous to that involved in wringing water from a wet towel; beyond a certain point no further water can be removed by sustained wringing. However, if the towel is unfolded and wrung out again then more water can be removed. In a screw press, this effect can be achieved by introduction of one or more humps and one or more mixers into the assembly. It  
25 is within the scope of the method of the present invention for the decompression/mixing to occur by use of a mixer, e.g. fitted to the worm shaft. However, preferably the mixer comprises of the combination of the Hump and Mixer. Pressure is built up initially by the combined action of helical worms and a tapered distance piece (or hump) and some fat is expelled. Pressure is then allowed  
30 to fall as the process material enters a mixing region, after which pressure is re-applied and more fat is expelled.

Furthermore, a measure of the compression can be described in terms of volume reduction (see figures 3a and 3b). Thus, a conventionally known mechanical screw press (figure 3a) will show a substantially constant volume reduction of the compressed material along the length of the worm assembly. This contrasts with the volume reduction observed with the method of the present invention. Due to the incorporation of a compression/mixing stage mounted in the worm assembly, the volume reduction is not constant. Indeed, at the point in the assembly where the mixer is positioned, an increase in the volume of the compressed material is observed. This may be an important feature of the present invention. The effect of these design modifications can be seen by comparing the Volume Reduction Curves for the two worm assemblies, from which the differences in pressure build-up along the press can be seen (Fig 3a & 3b).

Thus, according to an alternative aspect of the present invention we provide a method of extracting liquids from the process material which comprises the sequential steps of reducing the volume of the process material; increasing the volume of the process material; and reducing the volume of the process material in a mechanical screw press.

20

During trials of a DSR conversion of a Dupps press, it was also found that a further advantage was that there was no necessity to use the hydraulic choke to regulate pressure and there was much reduced burning and smoking of the residual cake. The performance improvements observed resulted from a fundamental analysis of the existing worm assembly and the judicious application of modifications to improve the flow and mixing of the process material. The pressure and/or speed of rotation of the worm, spacing between the worm and/or flights and the tunnel may be conventionally known *per se*. Thus, the press may optionally be provided with a choke, e.g. at the discharge end of the press. However, it is a particular advantage of the method of the invention that in many systems a choke is deemed unnecessary.

30

The method of the invention is advantageous in that, *inter alia*, an increased throughput of material is achieved. This increased throughput thus results in an increase in production rate with no detriment to the product quality.

- 5 The position of the compression mixer may vary according to the size and nature of the worm assembly, the material to be compressed, etc. However, in a preferred embodiment of the method of the invention, when the assembly is provided with a single compression mixer, the compression mixer is positioned close to the middle of the worm assembly, for example, at a position of between 40% and 70% of the length  
10 of the assembly, and preferably at between 50 and 65% of the length of the worm assembly, as measured from the feed inlet end. However, when the assembly is provided with more than one compression mixer, e.g. two compression mixers, they may be substantially evenly spaced along the length of the worm assembly. Thus, a first compression mixer may be positioned between 25 to 40% of the length of the  
15 worm assembly and a second compression mixer may be positioned between 60 and 80% of the length of the worm assembly.

The use of compression mixers in the extraction of oil from seeds etc is known.

- 20 Generally, the compression mixer comprises a tapered compression region and a mixer region. However, in the extraction of liquids from the process material, conventional mixers in the form of devices incorporating radially projecting elements e.g. in the form of a toothed disc, are unsuitable, due *inter alia*, to snagging, etc. Thus, the mixer may comprises an element adapted to disrupt the flow of material,  
25 this may be a multirecessed cog, a toothed disc, or any combination of the aforesaid. However, in the method of the invention a preferred mixer comprises a multirecessed cog.

- In one embodiment of the invention, the method may also include a temperature  
30 control element to facilitate flow. Thus, warming or heating the system may

facilitate flow of e.g. high melting fats at start up and, optionally, cooling may be used later in the process, thus further optimising fat extraction.

According to a further aspect of the invention, we provide a mechanical screw press  
5 comprising a worm assembly adapted to extract liquids from the process material by the sequential steps of compressing; decompressing and mixing; and recompressing the process material in a mechanical screw press.

According to a further aspect of the invention, we provide a mechanical screw press  
10 comprising a worm assembly provided with a plurality of circumferential flights and a compression mixer stage along the length of the worm assembly.

In this further aspect of the invention, the mechanical screw press may include a plurality of compression mixer stages.

15 Alternatively, we provide a mechanical screw press comprising a worm assembly adapted to extract liquids from process material by the sequential steps of volume reduction, volume increase and volume reduction.

20 The mechanical screw press of the invention comprises a worm assembly wherein the assembly is provided with at least one mixer region. Preferentially the mixer region is a combined compression/mixing region, e.g. a compression mixer as hereinbefore described.

25 We also provide the use of a worm assembly as hereinbefore described.

The use of the compression mixer in process material compression is also novel *per se*. Therefore according to a further aspect of the invention we provide the use of a compression mixer as hereinbefore described in the extraction of liquids from  
30 process material.

The invention will now be described by way of example only and with reference to the accompanying drawings in which Figure 1 is a representation of a Dupps screw press of the prior art;

Figure 2 is a representation of a modified Dupps screw press provided with a  
5 compression mixer region; and

Figures 3a and 3b are graphical representations of volume reduction curves produced from a prior art Dupps Screw press and a modified Dupps screw press.

Referring to Figure 1, a prior art arrangement (1) comprises a Cage (2) and worm  
10 assembly (3). The worm assembly (3) comprises a plurality of modular units (4) each fitted with an external flight (5). The press comprises a feed inlet end (6) and a discharge end (7).

Referring to Figure 2, the novel Arrangement (21) comprises a Cage (22) and worm  
15 assembly (23). The assembly (23) comprises a plurality of modular units (24) each fitted with an external flight (25). Close to the middle (28) of the worm assembly (23) a compressor/mixer (29) is positioned. The compressor mixer (29) comprises a frusto conical member (200) which is shaped to compress the process material (201) (not shown). The larger diameter end (202) of the frusto conical member (200) of the  
20 frusto conical member (200) is provided with a mixer (203). The mixer (203) is itself made up of a plurality of circumferential recesses (204) around the periphery (205) of the mixer.

In use, process material passes along the worm assembly due to the action of the  
25 flights. When the material reaches the compression mixer, the process material is further compressed and then allowed to expand in volume and mixed.

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**CLAIMS**

1. A method of extracting liquids from the process material which comprises the sequential steps of compressing the process material; decompressing and mixing the process material; and then recompressing the process material; in a mechanical screw press.  
5
2. A method of extracting liquids from the process material which comprises the sequential steps of reducing the volume of the process material; increasing the volume; and reducing the volume of the process material; in a mechanical screw press.  
10
3. A method according to claims 1 or 2 characterised in that the decompression and mixing step or the increasing volume step occurs separately, simultaneously or sequentially.  
15
4. A method according to claims 1 or 2 characterised in that an improvement in throughput is of in the region of 50% w/w.
- 20 5. A method according to claim 4 characterised in that the improvement in throughput is from 20 to 60%.
6. A method according to claim 5 characterised in that the improvement in throughput is from 30 to 50%.  
25
7. A method according to claims 1 or 2 characterised in that the extraction apparatus comprises an assembly of worms and/or flights in a tunnel provided with a feed end and a discharge end.
- 30 8. A method according to claim 7 characterised in that the worm assembly is provided with at least one mixer region.

9. A method according to claim 8 characterised in that the mixer region comprises a compressor/mixer region.
- 5 10. A method according to claim 8 characterised in that the mixer comprises an element adapted to disrupt the flow of material.
11. A method according to claim 8 characterised in that the mixer comprises a multirecessed cog, a toothed disc, or any combination of the aforesaid.
- 10 12. A method according to claim 11 characterised in that the mixer comprises a multirecessed cog.
13. A method according to claim 8 characterised in that the compressor  
15 comprises a frusto conical member.
14. A method according to claim 13 characterised in that the frusto conical member is smaller in diameter at the feed inlet end and greater in diameter at the discharge end.
- 20 15. A method according to claim 9 characterised in that the compression mixer is positioned at the discharge end.
16. A method according to claim 8 characterised in that the mixer is positioned  
25 close to the middle of the worm assembly.
17. A method according to claim 9 characterised in that the compression mixer is positioned close to the middle of the worm assembly.
- 30 18. A method according to claims 16 or 17 characterised in that the compression mixer is positioned at between 50 and 65% of the length of the worm assembly.

19. A method according to claim 18 characterised in that the compression mixer is positioned at between 50 to 60% of the length of the worm assembly as measured from the feed inlet end.
- 5
20. A method according to claim 8 characterised in that the worm is provided with a plurality of mixer regions.
21. A method according to claim 20 characterised in that the plurality of
- 10 compression mixers are substantially evenly spaced along the length of the worm assembly.
22. A method according to claim 21 characterised in that the first compression mixer is positioned between 25 to 40% of the length of the worm assembly; and a
- 15 second compression mixer is positioned between 60 and 80% of the length of the worm assembly.
23. A method according to claims 1 or 2 characterised in that the method includes a temperature control element to facilitate flow.
- 20
24. A method according to claim 3 characterised in that the extraction apparatus is provided with a choke.
25. A method according to claim 3 characterised in that the extraction apparatus
- 25 is not provided with a choke.
26. A mechanical screw press comprising a worm assembly adapted to extract liquids from the process material by the sequential steps of compressing; decompressing and mixing; and recompressing the process material.
- 30



27. A mechanical screw press comprising a worm assembly adapted to extract liquids from the process material by the sequential steps of volume reduction, volume increase; and volume reduction.
- 5 28. A mechanical screw press according to claims 26 or 27 characterised in that the decompression and mixing step or the increasing volume step occurs separately, simultaneously or sequentially.
29. A mechanical screw press according to claims 26 or 27 characterised in that  
10 an improvement in the throughput is of in the region of 50% w/w.
30. A mechanical screw press according to claim 29 characterised in that the improvement in throughput is from 20 to 60%.
- 15 31. A mechanical screw press according to claim 30 characterised in that the improvement in throughput is from 30 to 50%.
32. A mechanical screw press according to claims 26 or 27 characterised in that the extraction apparatus comprises an assembly of worms and/or flights in a tunnel  
20 provided with a feed end and a discharge end.
33. A mechanical screw press according to claims 26 or 27 characterised in that the worm assembly is provided with at least one mixer region.
- 25 34. A mechanical screw press according to claim 33 characterised in that the mixer region comprises a compression mixer.
35. A mechanical screw press according to claim 33 characterised in that the mixer comprises an element adapted to disrupt the flow of material.

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36. A mechanical screw press according to claim 35 characterised in that the mixer comprises a multirecessed cog, a toothed disc, or any combination of the aforesaid.
- 5 37. A mechanical screw press according to claim 36 characterised in that the compression mixer comprises a multirecessed cog.
38. A mechanical screw press according to claim 34 characterised in that the compressor comprises a frusto conical member.
- 10 39. A mechanical screw press according to claim 38 characterised in that the frusto conical member is smaller in diameter at the feed inlet end and greater in diameter at the discharge end.
- 15 40. A mechanical screw press according to claim 39 characterised in that the compression mixer is positioned at the discharge end.
41. A mechanical screw press according to claim 38 characterised in that the multirecessed cog is positioned at the discharge end of the frusto conical member.
- 20 42. A mechanical screw press according to claim 33 characterised in that the mixer is positioned close to the middle of the worm assembly.
43. A mechanical screw press according to claim 42 characterised in that the
- 25 compression mixer is positioned close to the middle of the worm assembly.
44. A mechanical screw press according to claims 42 or 43 characterised in that the compression mixer is positioned at between 50 and 65% of the length of the worm assembly.

30

45. A mechanical screw press according to claim 44 characterised in that the mixer region is positioned at between preferably 50 to 60% of the length of the worm assembly as measured from the feed inlet end.
- 5 46. A mechanical screw press according to claim 33 characterised in that the worm assembly is provided with a plurality of compression mixers.
47. A mechanical screw press according to claim 46 characterised in that the plurality of compression mixers is substantially evenly spaced along the length of the  
10 worm assembly.
48. A mechanical screw press according to claim 47 characterised in that the first compression mixer is positioned between 25 to 40% of the length of the worm assembly; and a second compression mixer is positioned between 60 and 80% of the  
15 length of the worm assembly.
49. A mechanical screw press according to claims 26 or 27 characterised in that the press is adapted to include a temperature control element to facilitate flow.
- 20 50. A mechanical screw press according to claims 26 or 27 characterised in that the extraction apparatus is provided with a choke.
51. A mechanical screw press according to claims 26 or 27 characterised in that the extraction apparatus is not provided with a choke.  
25
52. The use of a mechanical screw press according to claims 26 or 27 in the extraction of liquids from the process material.
53. The use of a compression mixer in the extraction of liquids from the process  
30 material.

54. A method or mechanical screw press substantially as described with reference to the accompanying drawings.

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**Abstract****5 Improvements to Rendering Presses**

There is described a method of extracting liquids from the process material which comprises the sequential steps of compressing the process material; decompressing and mixing the process material; and then recompressing the process material; in a  
10 mechanical screw press.

There is also described a mechanical screw press comprising a worm assembly adapted to extract liquids using the aforementioned process.

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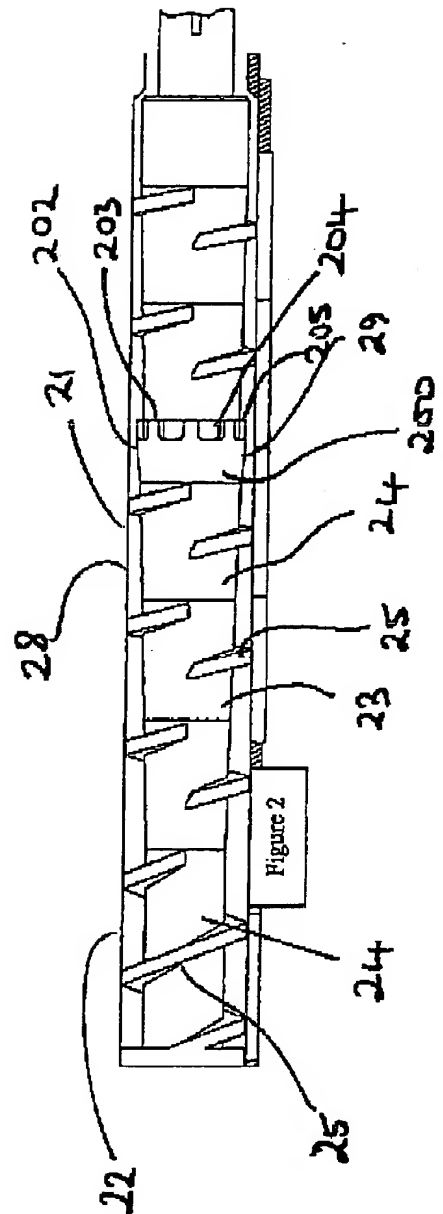
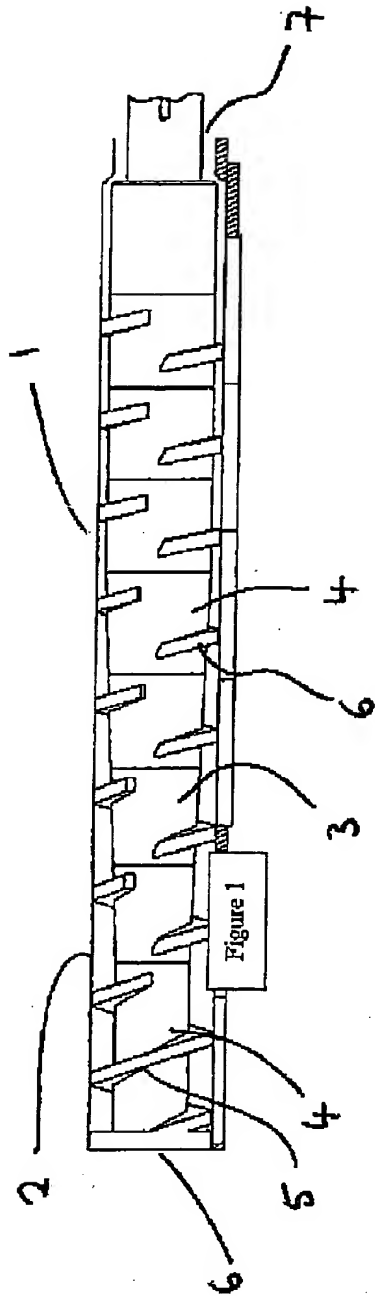
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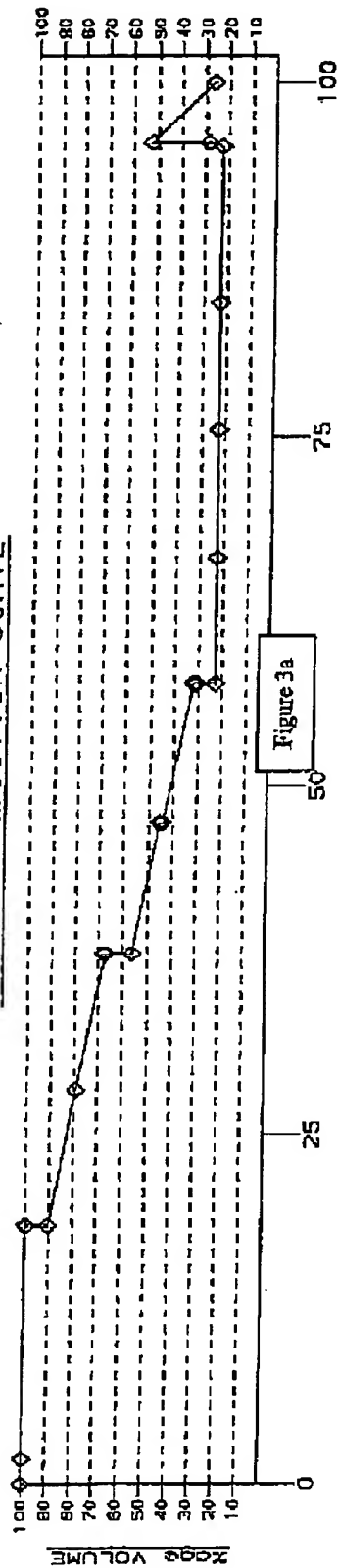
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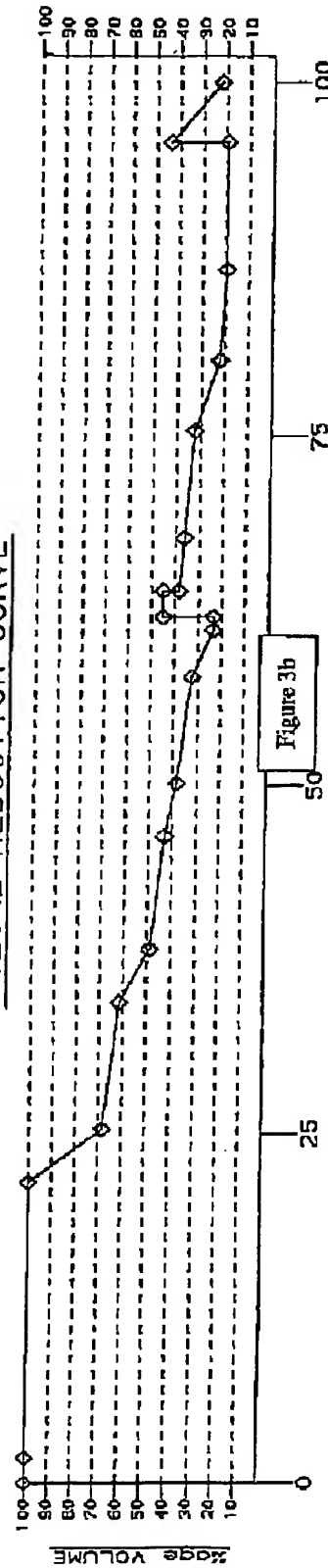
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